



08/120105

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HOE 92/F 294

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## Description

Polyolefin molding composition having a broad melting range, process for its preparation, and its use

- 5 As a rule, metallocene/aluminoxane catalyst systems allow the preparation of polyolefins or polyolefin copolymers having a sharp melting point. These products are highly suitable, for example, for thin-wall injection molding or precision injection molding, giving very short cycle
- 10 times per injection-molded part.

- By contrast, many applications, for example thermoforming, blow molding, extrusion, injection stretch blow molding and certain film applications are unsuitable for a polyolefin having such a sharp melting and crystallization range.
- 15

- In thermoforming, a product of this type leads to process problems and, for example, moldings having uneven wall thicknesses. In film applications, heat-sealing or stretching, for example, is difficult with a product
- 20 having a sharp melting point. Such applications require a polyolefin having a broad melting range.

- The object was to find a process which enables the preparation of polyolefin molding compositions having a broad melting range. The object has been achieved by
- 25 polymerization or copolymerization of the olefin or olefins by means of at least two different metallocenes.

- At a certain polymerization temperature, a polyolefin having a certain melting point is formed due to the stereospecificity of each type of metallocene catalyst.
- 30 Surprisingly, it has now been found that a mixture of at least two metallocenes each of which gives polyolefins of very different melting points give a polyolefin mixture

which does not, as expected, have a mixed melting point or a melting point below the melting point of the lower-melting component, but instead gives a polymer product which has two melting points. The melting range determined by means of the DSC ("differential scanning calorimeter") spectrum is, in direct comparison with the separate polymers, significantly broadened or even bimodal, and the product has the above-discussed advantages on conversion into moldings.

10 In addition it has been found that the mixing of polyolefins having different melting points, for example by extrusion, likewise gives a product which has a broad bimodal or multimodal melting range.

The invention thus relates to the preparation of a polyolefin molding composition having the following properties:

The molding composition has a broad, bimodal or multimodal melting range in the DSC spectrum. The melting range maximum is between 120 and 165°C, the half-intensity width of the melting peak is broader than 10°C, and the width determined at the quarter peak height is greater than 15°C. In addition, the half-intensity width of the crystallization peak is greater than 4°C and the width of the crystallization peak determined at the quarter peak height is greater than 6°C.

Fractional crystallization or extraction with hydrocarbons allows the molding composition to be separated into its components, and the resultant polyolefin components have relatively sharp melting and crystallization peaks.

In addition to the polyolefin, the molding composition according to the invention may also contain conventional additives, for example nucleating agents, stabilizers, antioxidants, UV absorbers, light stabilizers, metal deactivators, free-radical scavengers, fillers and

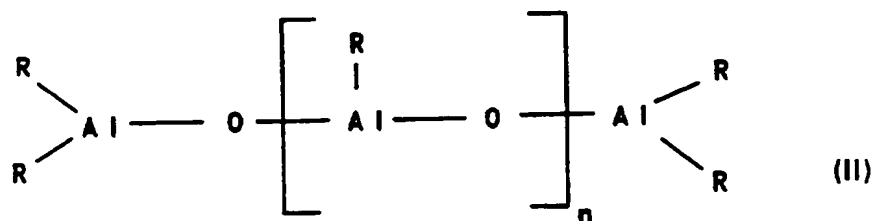
reinforcing agents, compatibilizers, plasticizers, lubricants, emulsifiers, pigments, optical brighteners, flameproofing agents, antistatics and blowing agents.

This novel polyolefin molding composition is prepared

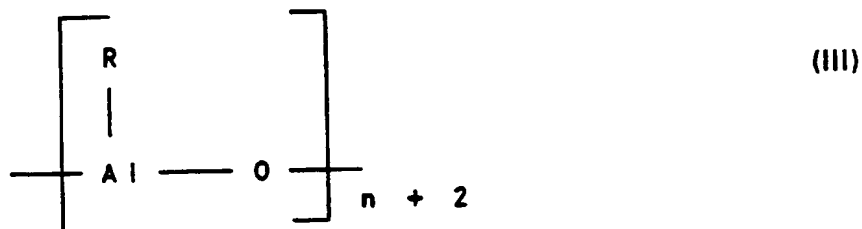
- 5 a) by mixing at least two, preferably two or three, polyolefins of different melting points. The melting points of at least two of the polyolefins must differ by at least 5°C. There are no restrictions on the mixing ratio of the polyolefins nor on the  
10 molecular weight dispersity. The viscosity index should be greater than  $VI = 10 \text{ cm}^3/\text{g}$ , and the molecular weight  $M_w$  should be greater than 5000 g/mol. The polymers can be mixed by one of the methods conventional in plastics processing. One possibility  
15 is sintering in a high-speed mixer if the polymers to be mixed are pulverulent, and another possibility is the use of an extruder having mixing and compounding elements on the screw, or the use of a compounder as used in the rubber industry, or
- 20 b) by direct polymerization of at least two, preferably two or three, polyolefins of different melting point. The melting points of at least two of the polyolefins must differ by at least 5°C. There are no restrictions on the mixing ratio of the poly-  
25 olefins prepared in the polymerization.

This direct polymerization of the polyolefin molding composition according to the invention is carried out by polymerization or copolymerization of olefins of the formula  $R^a\text{CH}=\text{CHR}^b$ , in which  $R^a$  and  $R^b$  are identical or  
30 different and are a hydrogen atom or an alkyl radical having 1 to 14 carbon atoms, or  $R^a$  and  $R^b$ , together with the atoms connecting them, can form a ring, at a temperature of from -60 to 200°C, a pressure of from 0.5 to 100 bar, in solution, in suspension or in the gas phase,  
35 in the presence of a catalyst which comprises at least

two transition-metal components (metallocenes) and an aluminoxane of the formula II

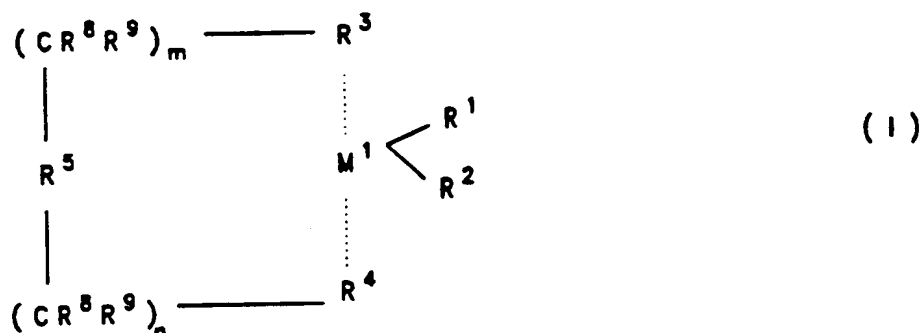


for the linear type and/or of the formula III



for the cyclic type, where, in the formulae II and III, the radicals R may be identical or different and are a C<sub>1</sub>-C<sub>6</sub>-alkyl group, a C<sub>1</sub>-C<sub>6</sub>-fluoroalkyl group, a C<sub>6</sub>-C<sub>18</sub>-aryl group, a C<sub>6</sub>-C<sub>18</sub>-fluoroaryl group or hydrogen, and n is an integer from 0 to 50, and the aluminoxane component may additionally contain a compound of the formula AlR<sub>3</sub>,

where the transition-metal component used comprises at least two metallocenes of the formula I:



in which

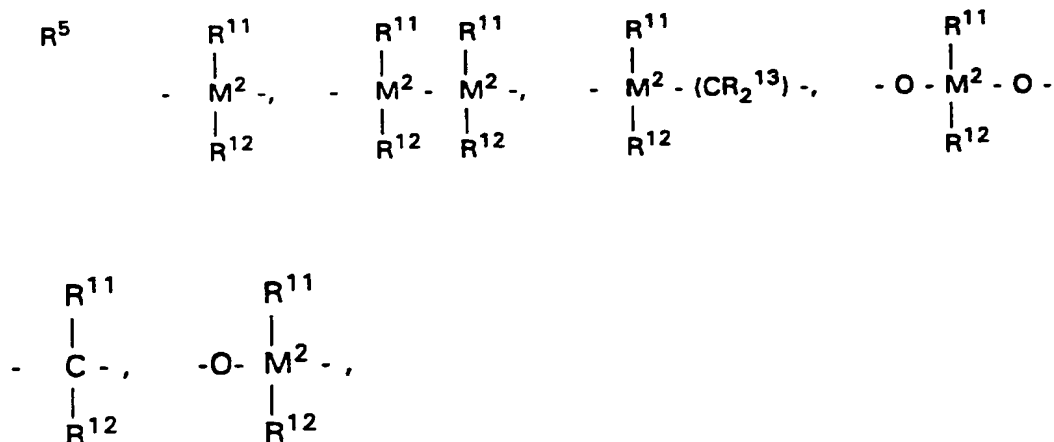
M<sup>1</sup> is Zr, Hf or Ti,

R<sup>1</sup> and R<sup>2</sup> are identical or different and are a hydrogen atom, a C<sub>1</sub>-C<sub>10</sub>-alkyl group, a C<sub>1</sub>-C<sub>10</sub>-alkoxy group, a C<sub>6</sub>-C<sub>10</sub>-aryl group, a C<sub>6</sub>-C<sub>10</sub>-aryloxy group, a C<sub>2</sub>-C<sub>10</sub>-alkenyl group, a C<sub>7</sub>-C<sub>40</sub>-arylalkyl group, a

C<sub>7</sub>-C<sub>40</sub>-alkylaryl group, a C<sub>8</sub>-C<sub>40</sub>-arylalkenyl group or a halogen atom,

R<sup>3</sup> and R<sup>4</sup> are identical or different and are a monocyclic or polycyclic, unsubstituted or substituted hydrocarbon radical which, together with the metal atom M<sup>1</sup>, can form a sandwich structure,

R<sup>5</sup> is



=BR<sup>11</sup>, =AlR<sup>11</sup>, -Ge-, -Sn-, -O-, -S-, =SO, =SO<sub>2</sub>, =NR<sup>11</sup>, =CO, =PR<sup>11</sup> or =P(O)R<sup>11</sup>,

where

R<sup>11</sup>, R<sup>12</sup> and R<sup>13</sup> are identical or different and are a hydrogen atom, a halogen atom, a C<sub>1</sub>-C<sub>10</sub>-alkyl group, a C<sub>1</sub>-C<sub>10</sub>-fluoroalkyl group, a C<sub>6</sub>-C<sub>10</sub>-aryl group, a C<sub>6</sub>-C<sub>10</sub>-fluoroaryl group, a C<sub>1</sub>-C<sub>10</sub>-alkoxy group, a C<sub>2</sub>-C<sub>10</sub>-alkenyl group, a C<sub>7</sub>-C<sub>40</sub>-arylalkyl group, a C<sub>8</sub>-C<sub>40</sub>-arylalkenyl group or a C<sub>7</sub>-C<sub>40</sub>-alkylaryl group, or R<sup>11</sup> and R<sup>12</sup> or R<sup>11</sup> and R<sup>13</sup>, in each case together with the atoms connecting them, form a ring, and M<sup>2</sup> is silicon, germanium or tin,

R<sup>8</sup> and R<sup>9</sup> are identical or different and are as defined for R<sup>11</sup>,

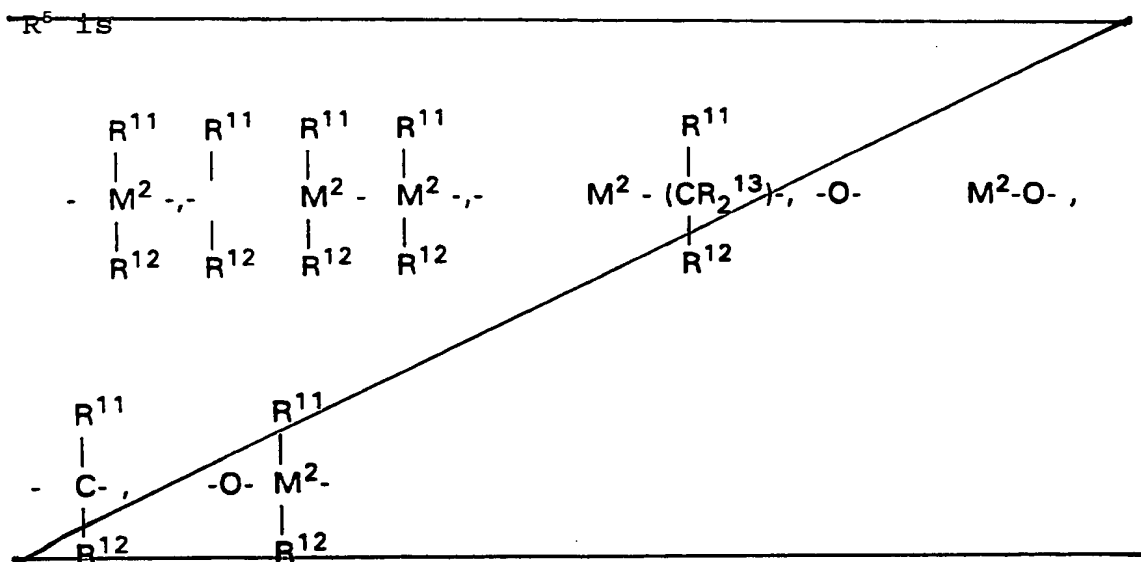
m and n are identical or different and are zero, 1 or 2, where m plus n is zero, 1 or 2.

Alkyl is straight-chain or branched alkyl. Halogen (halogenated) denotes fluorine, chlorine, bromine or iodine, preferably fluorine or chlorine.

M<sup>1</sup> is Zr, Hf or Ti, preferably Zr or Hf.

R<sup>1</sup> and R<sup>2</sup> are identical or different and are a hydrogen atom, a C<sub>1</sub>-C<sub>10</sub>-, preferably C<sub>1</sub>-C<sub>3</sub>-alkyl group, a C<sub>1</sub>-C<sub>10</sub>-, preferably C<sub>1</sub>-C<sub>3</sub>-alkoxy group, a C<sub>6</sub>-C<sub>10</sub>-, preferably C<sub>6</sub>-C<sub>8</sub>-aryl group, a C<sub>6</sub>-C<sub>10</sub>-, preferably C<sub>6</sub>-C<sub>8</sub>-aryloxy group, a C<sub>2</sub>-C<sub>10</sub>-, preferably C<sub>2</sub>-C<sub>4</sub>-alkenyl group, a C<sub>7</sub>-C<sub>40</sub>-, preferably C<sub>7</sub>-C<sub>10</sub>-arylalkyl group, a C<sub>7</sub>-C<sub>40</sub>-, preferably C<sub>7</sub>-C<sub>12</sub>-alkylaryl group, a C<sub>8</sub>-C<sub>40</sub>-, preferably C<sub>8</sub>-C<sub>12</sub>-arylalkenyl group or a halogen atom, preferably chlorine.

10 R<sup>3</sup> and R<sup>4</sup> are identical or different monocyclic or polycyclic, unsubstituted or substituted hydrocarbon radicals which, together with the metal atom M<sup>1</sup>, can form a sandwich structure.



15 =BR<sup>11</sup>, =AlR<sup>11</sup>, -Ge-, -Sn-, -O-, -S-, =SO, =SO<sub>2</sub>, =NR<sup>11</sup>, =CO, =PR<sup>11</sup> or =P(O)R<sup>11</sup>, where R<sup>11</sup>, R<sup>12</sup> and R<sup>13</sup> are identical or different and are a hydrogen atom, a halogen atom, a C<sub>1</sub>-C<sub>10</sub>-, preferably C<sub>1</sub>-C<sub>4</sub>-alkyl group, in particular a methyl group, a C<sub>1</sub>-C<sub>10</sub>-fluoroalkyl group, preferably a CF<sub>3</sub> group, a C<sub>6</sub>-C<sub>10</sub>-, preferably C<sub>6</sub>-C<sub>8</sub>-aryl group, a C<sub>6</sub>-C<sub>10</sub>-fluoroaryl group, preferably a pentafluorophenyl group, a C<sub>1</sub>-C<sub>10</sub>-, preferably C<sub>1</sub>-C<sub>4</sub>-alkoxy group, in particular a methoxy group, a C<sub>2</sub>-C<sub>10</sub>-, preferably C<sub>2</sub>-C<sub>4</sub>-alkenyl group, a C<sub>7</sub>-C<sub>40</sub>-, preferably C<sub>7</sub>-C<sub>10</sub>-arylalkyl group, a C<sub>8</sub>-C<sub>40</sub>-,

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preferably C<sub>8</sub>-C<sub>12</sub>-arylalkenyl group or a C<sub>7</sub>-C<sub>40</sub>-, preferably C<sub>7</sub>-C<sub>12</sub>-alkylaryl group, or R<sup>11</sup> and R<sup>12</sup> or R<sup>11</sup> and R<sup>13</sup>, in each case together with the atoms connecting them, form a ring.

- 5 M<sup>2</sup> is silicon, germanium or tin, preferably silicon or germanium.

R<sup>5</sup> is preferably =CR<sup>11</sup>R<sup>12</sup>, =SiR<sup>11</sup>R<sup>12</sup>, =GeR<sup>11</sup>R<sup>12</sup>, -O-, -S-, =SO, =PR<sup>11</sup> or =P(O)R<sup>11</sup>.

- 10 R<sup>8</sup> and R<sup>9</sup> are identical or different and are as defined for R<sup>11</sup>.

m and n are identical or different and are zero, 1 or 2, preferably zero or 1, where m plus n is zero, 1 or 2, preferably zero or 1.

- 15 Particularly preferred metallocenes are thus those in which M<sup>1</sup> is zirconium or hafnium, R<sup>1</sup> and R<sup>2</sup> are identical and are methyl or chlorine, R<sup>4</sup> and R<sup>3</sup> are indenyl, cyclopentadienyl or fluorenyl, where these ligands may carry additional substituents as defined for R<sup>11</sup>, R<sup>12</sup> and R<sup>13</sup>, where the substituents may be different and, with the  
20 atoms connecting them, may also form rings,

R<sup>5</sup> is a



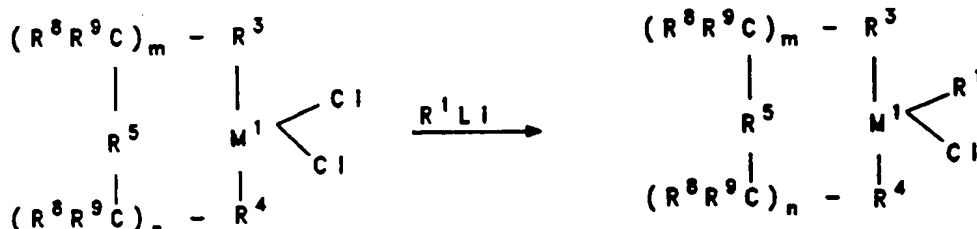
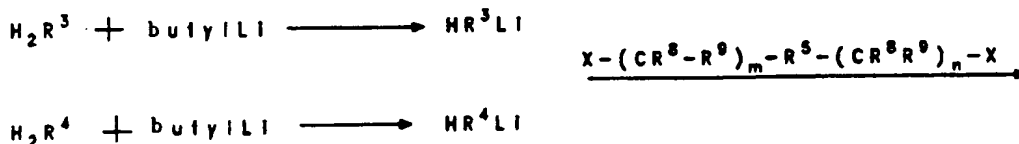
radical, and n plus m is zero or 1, in particular the compounds listed in the working examples.

- 25 The chiral metallocenes are employed as a racemate for the preparation of highly isotactic polyolefins. However, the pure R or S form can also be used. These pure

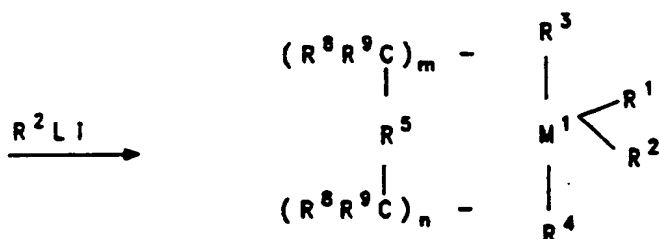
stereoisomeric forms can be used to prepare an optically active polymer. However, the meso form of the metallocenes can be separated off, since the polymerization-active center (the metal atom) in these compounds is no longer chiral due to mirror symmetry at the central metal and a highly isotactic polymer therefore cannot be produced. If the meso form is not separated off, atactic polymer is formed in addition to isotactic polymer. For certain applications - soft moldings for example - this may be entirely desirable. Metallocenes having a formal  $C_s$  symmetry are suitable for the preparation of syndiotactic polyolefins.

The separation of the stereoisomers is known in principle.

In principle, the metallocenes I can be prepared by the following reaction scheme:







X = Cl, Br, I, O-Tosyl;

The preparation of the metallocene compounds is known.

The DSC measurements on the polyolefin composition according to the invention are preferably carried out at  
5 a heating or cooling rate of  $\leq 20^\circ\text{C}/\text{min}$ .

The choice of metallocenes for the polymerization of olefins to give polyolefins having a broad, bimodal or multimodal melting range can in each case take place by means of a test polymerization per metallocene.

- 10 In this test, the olefin is polymerized to the polyolefin and its melting curve determined by DSC analysis. The metallocenes are then combined depending on the desired melting range with respect to melting range maximum and melting range width.
- 15 Taking into account the polymerization activities, computer simulation of the combined DSC curves makes it possible to adjust each desired melting curve type via the type of metallocenes and via the mixing ratio of the metallocenes with one another.
- 20 The number of metallocenes I to be used according to the invention in the polymerization is preferably 2 or 3, in particular 2. However, it is also possible to employ a larger number (such as, for example, 4 or 5) in any desired combination.

Taking into account the polymerization activities and molecular weights at various polymerization temperatures, in the presence of hydrogen as molecular weight regulator or in the presence of comonomers, the computer simulation  
5 model can be further refined and the applicability of the process according to the invention further improved.

The cocatalyst used is an aluminoxane of the formula II and/or III, in which  $n$  is an integer from 0 to 50, preferably from 10 to 35.

10 The radicals  $R$  are preferably identical and are methyl, isobutyl, phenyl or benzyl, particularly preferably methyl.

If the radicals  $R$  are different, they are preferably methyl and hydrogen or alternatively methyl and isobutyl,  
15 where hydrogen or isobutyl is preferably present to the extent of 0.01 - 40% (number of radicals  $R$ ). Instead of the aluminoxane, the cocatalyst used in the polymerization can be a mixture comprising the aluminoxane and  $AlR_3$ , where  $R$  is as defined above.

20 The aluminoxane can be prepared in various ways by known processes. One of the methods is, for example, to react an aluminum hydrocarbon compound and/or a hydridoaluminum hydrocarbon compound with water (in gas, solid, liquid or bonded form, for example as water of crystallization) in  
25 an inert solvent (such as, for example, toluene). In order to prepare an aluminoxane containing different alkyl groups  $R$ , two different trialkylaluminum compounds ( $AlR_3 + AlR'_3$ ) in accordance with the desired composition are reacted with water (cf. S. Pasynkiewicz, Polyhedron  
30 9 (1990) 429 and EP-A 302 424).

The precise structure of the aluminoxanes II and III is unknown.

Depending on the type of preparation, all aluminoxane

solutions have in common a varying content of unreacted aluminum starting compound, which is in free form or as an adduct.

5 It is possible to preactivate the metallocenes before use in the polymerization reaction, in each case separately or together as a mixture with an aluminoxane of the formula (II) and/or (III). This significantly increases the polymerization activity and improves the grain morphology.

10 The preactivation of the metallocenes is carried out in solution. The metallocenes are preferably dissolved, as a solid, in a solution of the aluminoxane in an inert hydrocarbon. Suitable inert hydrocarbons are aliphatic and aromatic hydrocarbons. Preference is given to toluene  
15 or a C<sub>6</sub>-C<sub>10</sub>-hydrocarbon.

The concentration of the aluminoxane in the solution is in the range from about 1% by weight to the saturation limit, preferably from 5 to 30% by weight, in each case  
20 based on the total solution. The metallocenes can be employed in the same concentration, but are preferably employed in an amount of from 10<sup>-4</sup> to 1 mol per mol of aluminoxane. The preactivation time is from 5 minutes to 60 hours, preferably from 5 to 60 minutes. The temperature is from -78 to 100°C, preferably from 0 to 70°C.

25 The metallocenes can also be prepolymerized or applied to a support. For prepolymerization, the (or one of the) olefin(s) employed in the polymerization is preferably used.

30 Examples of suitable supports are silica gels, aluminum oxides, solid aluminoxane, combinations of aluminoxane on a support, such as, for example, silica gel or other inorganic support materials. Another suitable support material is a polyolefin powder in finely divided form.

A further possible embodiment of the process according to the invention comprises using a salt-like compound of the formula  $R_xNH_{4-x}BR'_4$  or of the formula  $R_3PHBR'_4$  as cocatalyst in place of or in addition to an aluminoxane. In these  
5 formulae, x is 1, 2 or 3, R is identical or different and is alkyl or aryl, and R' is aryl, which may also be fluorinated or partly fluorinated. In this case, the catalyst comprises the product of the reaction of the metallocenes with one of said compounds (cf.  
10 EP-A 277 004).

In order to remove catalyst poisons present in the olefin, purification by means of an alkylaluminum compound, for example  $AlMe_3$  or  $AlEt_3$ , is advantageous. This  
15 purification can be carried out either in the polymerization system itself, or the olefin is brought into contact with the Al compound before addition to the polymerization system and subsequently removed again.

The polymerization or copolymerization is carried out in a known manner in solution, in suspension or in the gas  
20 phase, continuously or batchwise, in one or more steps, at a temperature of from  $-60$  to  $200^\circ C$ , preferably from  $20$  to  $80^\circ C$ . Olefins of the formula  $R^a-CH=CH-R^b$  are polymerized or copolymerized. In this formula,  $R^a$  and  $R^b$  are identical or different and are a hydrogen atom or an  
25 alkyl radical having 1 to 14 carbon atoms. However,  $R^a$  and  $R^b$  may also form a ring together with the carbon atoms connecting them. Examples of such olefins are ethylene, propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, 1-octene, norbornene and norbornadiene. In  
30 particular, propylene and ethylene are polymerized.

If necessary, hydrogen is added as molecular weight regulator.

The total pressure in the polymerization system is from 0.5 to 100 bar. The polymerization is preferably carried  
35 out in the industrially particularly relevant pressure

range of from 5 to 64 bar.

The metallocenes are used in a concentration, based on the transition metal, of from  $10^{-3}$  to  $10^{-8}$  mol, preferably from  $10^{-4}$  to  $10^{-7}$  mol, of transition metal per  $\text{dm}^3$  of solvent or per  $\text{dm}^3$  of reactor volume. The aluminoxane or the aluminoxane/ $\text{AlR}_3$  mixture is used in a concentration of from  $10^{-5}$  to  $10^{-1}$  mol, preferably from  $10^{-4}$  to  $10^{-2}$  mol, per  $\text{dm}^3$  of solvent or per  $\text{dm}^3$  of reactor volume. In principle, however, higher concentrations are also possible.

If the polymerization is carried out as a suspension or solution polymerization, an inert solvent which is customary for the Ziegler low-pressure process is used. For example, the polymerization is carried out in an aliphatic or cycloaliphatic hydrocarbon, examples which may be mentioned being butane, pentane, hexane, heptane, decane, isooctane, cyclohexane and methylcyclohexane.

It is furthermore possible to use a benzine or hydrogenated diesel oil fraction. Toluene can also be used. The polymerization is preferably carried out in the liquid monomer.

If inert solvents are used, the monomers are metered in as gases or liquids.

The polymerization can have any desired duration, since the catalyst system to be used according to the invention exhibits only a slight time-dependent drop in polymerization activity.

The process according to the invention is distinguished by the fact that the metallocenes described give polymers having a broad, bimodal or multimodal melting range in the industrially relevant temperature range of between 20 and  $80^\circ\text{C}$  and with high polymerization activity.

The polyolefin molding compositions according to the invention are particularly suitable for the production of moldings by thermoforming, blow molding, extrusion, injection stretch blow molding and for certain film applications, such as heat-sealing or stretching.

The examples below serve to illustrate the invention in greater detail.

The following abbreviations are used:

VI = viscosity index in  $\text{cm}^3/\text{g}$   
10  $M_w$  = weight average molecular weight in  $\text{g/mol}$  } determined by gel permeation chromatography  
 $M_w/M_n$  = molecular weight dispersity)  
MFI (230/5) = melt flow index, measured according to DIN 53735, at a melt temperature of  $230^\circ\text{C}$   
15 and with a weight of 5 kg.

Melting points, peak widths, melting ranges and crystallization temperatures were determined by DSC spectrometry (heating/cooling rate  $20^\circ\text{C}/\text{min}$ ).

#### Example 1

20 In each case 5 kg of two different polypropylene powders were mixed, stabilized against chemical degradation under extrusion conditions by means of 20 g of pentaerythrityl tetrakis[3-(3,5-di-*t*-butyl-4-hydroxyphenyl)propionate], extruded in a ZSK 28 twin-screw extruder (Werner und  
25 Pfleiderer) and subsequently granulated. The temperatures in the heating zones were  $150^\circ\text{C}$  (feed),  $210^\circ\text{C}$ ,  $250^\circ\text{C}$ ,  $280^\circ\text{C}$  and  $215^\circ\text{C}$  (die plate), the material temperature in the extruder was  $275^\circ\text{C}$ , and the extruder screws rotated at 250 rpm. The base polymers used for the mixture had  
30 the following properties:

Polymer 1: VI =  $255 \text{ cm}^3/\text{g}$ ; MFI (230/5) = 6.8 dg/min;  $M_w$  = 310,000 g/mol;  $M_w/M_n$  = 2.2; melting point (melting peak

maximum) 139°C, half-intensity width of the melting peak 5°C, width at quarter peak height 16°C; crystallization point 101°C, half-intensity width of the crystallization peak 4.0°C, width at quarter peak height 5.5°C.

- 5 Polymer 2: VI = 235 cm<sup>3</sup>/g; MFI (230/5) = 10 dg/min; M<sub>w</sub> = 277,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.3; melting point (melting peak maximum) 152°C, half-intensity width of the melting peak 8°C, width at quarter peak height 12°C; crystallization point 105°C, half-intensity width of the crystallization peak 6°C, width at quarter peak height 7.5°C.

The novel molding composition prepared by extrusion had the following data:

- 15 VI = 257 cm<sup>3</sup>/g; MFI (230/5) = 8.7 dg/min; M<sub>w</sub> = 300,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.8; melting range maximum at 150°C, shoulder at 130°C; half-intensity width of the melting peak 19°C, width at quarter peak height 31°C; crystallization peak maximum 105°C; half-intensity width of crystallization peak 8.5°C, width at quarter peak height 11.5°C.

20 Example 2

Example 1 was repeated, but two other polypropylene components were used and the extruder parameters were 130°C (feed), 155°C, 200°C, 250°C and 250°C (die plate), material temperature 225°C, extruder screw speed 300 rpm.

- 25 Polymer 1: VI = 155 cm<sup>3</sup>/g; MFI (230/5) = 65 dg/min; M<sub>w</sub> = 172,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.8; melting point (melting peak maximum) 137°C, half-intensity width of the melting peak 10°C, width at quarter peak height 17°C; crystallization point 104°C, half-intensity width of the crystallization peak 5°C, width at quarter peak height 7.5°C.

Polymer 2: VI = 156 cm<sup>3</sup>/g; MFI (230/5) = 68 dg/min; M<sub>w</sub> = 153,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.1; melting point (melting peak

maximum) 153°C, half-intensity width of the melting peak 7.5°C, width at quarter peak height 18.8°C; crystallization point 110°C, half-intensity width of the crystallization peak 5°C, width at quarter peak height 7.5°C.

5 Novel molding composition prepared therefrom:

VI = 158 cm<sup>3</sup>/g; MFI (230/5) = 67 dg/min;  $M_w$  = 168,000 g/mol;  $M_w/M_n$  = 2.6; melting range maximum at 148°C, shoulder at 138°C; half-intensity width 19°C, width at quarter peak height 31°C; crystallization peak maximum 112°C; half-intensity width of crystallization peak 6°C, width at quarter peak height 10.5°C.

### Example 3

Example 1 was repeated, but two other polypropylene components were used and the extruder parameters were 150°C (feed), 160°C, 240°C, 240°C and 240°C (die plate), material temperature 250°C, extruder screw speed 220 rpm.

Polymer 1: VI = 407 cm<sup>3</sup>/g; MFI (230/5) = 1.9 dg/min;  $M_w$  = 488,000 g/mol;  $M_w/M_n$  = 2.2; melting point (melting peak maximum) 158°C, half-intensity width of the melting peak 8°C, width at quarter peak height 15°C; crystallization point 109°C, half-intensity width of the crystallization peak 6.5°C, width at quarter peak height 9.5°C.

Polymer 2: VI = 132 cm<sup>3</sup>/g; MFI (230/5) = 93 dg/min; melting point (melting peak maximum) 138°C, half-intensity width of the melting peak 7°C, width at quarter peak height 18°C; crystallization peak (maximum) 99°C, half-intensity width of the crystallization peak 6.5°C, width at quarter peak height 8°C.

Novel molding composition prepared therefrom:

30 VI = 247 cm<sup>3</sup>/g; MFI (230/5) = 12.3 dg/min;  $M_w$  = 268,000 g/mol;  $M_w/M_n$  = 3.0; melting range maximum at 154°C, shoulder at 141°C; half-intensity width 15°C,



width at quarter peak height 29°C; crystallization at 114°C.

#### Example 4

Example 3 was repeated, but the polymer component 2 used therein was replaced by a polypropylene having the following data:

VI = 353 cm<sup>3</sup>/g; MFI (230/5) = 2.1 dg/min;  
M<sub>w</sub> = 465,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.1; melting point (melting peak maximum) 153°C, half-intensity width of the melting peak 9.5°C, width at quarter peak height 13.5°C; crystallization point 110°C, half-intensity width of the crystallization peak 7.5°C, width at quarter peak height 9°C.

Novel molding composition prepared therefrom:

VI = 366 cm<sup>3</sup>/g; MFI (230/5) = 1.9 dg/min;  
M<sub>w</sub> = 486,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.1; double melting range maximum at 157 and 159°C, half-intensity width 17.5°C, width at quarter peak height 29°C; crystallization at 115°C, width at quarter peak height 11°C.

#### Example 5

The procedure was as in Example 1, but 5 kg of polymer 1 from Example 3 and 10 kg of polymer 1 from Example 1 were used. The extruder parameters were 150°C (feed), 160°C, 250°C, 250°C and 240°C (die plate), material temperature 255°C, extruder screw speed 190 rpm.

The novel molding composition prepared from these two polymer components had the following data:

VI = 302 cm<sup>3</sup>/g; MFI (230/5) = 4.2 dg/min;  
M<sub>w</sub> = 366,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.5; melting range maximum 151°C, half-intensity width 18°C, width at quarter peak height 34.5°C, crystallization at 106°C with a signal half-intensity width of 7.5°C and a width at quarter peak

height of 10.5°C.

#### Example 6

A dry 150 dm<sup>3</sup> reactor was flushed with propylene and charged at 20°C with 80 dm<sup>3</sup> of a benzine fraction having the boiling range 100-120°C from which the aromatic components had been removed, 50 dm<sup>3</sup> of liquid propylene and 150 cm<sup>3</sup> of a toluene solution of methylaluminoxane (corresponding to 250 mmol of Al, molecular weight according to hygroscopic determination 1050 g/mol). The temperature was then adjusted to 40°C. A hydrogen content of 0.05% by volume was set in the gas phase (the content was kept constant during the polymerization by continual topping up of hydrogen). 7.5 mg of a rac-Me<sub>2</sub>Si(2-methyl-1-indenyl)<sub>2</sub>ZrCl<sub>2</sub> and 45 mg of a rac-Me<sub>2</sub>Si(indenyl)<sub>2</sub>HfCl<sub>2</sub> were mixed, and the solid was dissolved in 25 cm<sup>3</sup> of a toluene solution of methylaluminoxane (42 mmol of Al) and introduced into the reactor after 15 minutes. The polymerization system was kept at 43°C for 24 hours by cooling. Polymerization was terminated by addition of 2.5 bar of CO<sub>2</sub> gas and the polymer formed (22.6 kg) was separated from the suspension medium in a pressure filter. The product was dried for 24 hours at 80°C/200 mbar. 50 g of pentaerythrityl tetrakis[3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate] were added to the polymer powder to prevent chemical degradation, and the mixture was extruded in a ZSK 28 twin-screw extruder (Werner und Pfleiderer) and then granulated. The temperatures in the heating zones were 150°C (feed), 200°C, 240°C, 250°C (die plate), the extruder screw speed was 200 rpm, and the material temperature was 250°C.

The novel molding composition had the following data:  
VI = 285 cm<sup>3</sup>/g; MFI (230/5) = 5.4 dg/min;  
M<sub>w</sub> = 334,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.2; melting range maximum at 152°C, shoulder at 132°C, half-intensity width of the melting peak 17.5°C, width at quarter peak height 35°C; crystallization peak maximum 106°C; half-intensity width

of crystallization peak 8.5°C; width at quarter peak height 12.5°C.

#### Example 7

Example 6 was repeated, but the metallocenes used were  
5 7.5 mg of phenyl(methyl)Si(2-methyl-1-indenyl)<sub>2</sub>ZrCl<sub>2</sub> and  
2.5 mg of Me<sub>2</sub>Si(2-methyl-4-phenyl-1-indenyl)<sub>2</sub>ZrCl<sub>2</sub>, the  
polymerization temperature was 48°C and a hydrogen  
content of 2.5% by volume was set in the gas phase.  
21.5 kg of polymer were obtained. The molding composition  
10 obtained after extrusion and granulation had the follow-  
ing properties:

VI = 194 cm<sup>3</sup>/g; MFI (230/5) = 28.8 dg/min;  
M<sub>w</sub> = 238,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.8; melting range maximum at  
157°C, half-intensity width 13.5°C, width at quarter peak  
15 height 24°C; crystallization peak maximum 115°C; half-  
intensity width 6.5°C; width at quarter peak height  
9.5°C.

The molding composition was separated into two consti-  
tuents semi-quantitatively by fractional crystallization.

20 Polymer 1 made up about 45% by weight and had the follow-  
ing data:

VI = 179 cm<sup>3</sup>/g; MFI (230/5) = 34 dg/min;  
M<sub>w</sub> = 195,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.1; melting point (melting  
peak maximum) 151°C, half-intensity width 8.5°C, crystal-  
25 lization peak 111°C; half-intensity width 4°C.

Polymer 2 made up about 55% by weight and had the follow-  
ing data:

VI = 207 cm<sup>3</sup>/g; MFI (230/5) = 27 dg/min;  
M<sub>w</sub> = 259,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.5; melting point (melting  
30 peak maximum) 159°C, half-intensity width 5°C, width at  
quarter peak height 12.5°C; crystallization peak at  
117°C; half-intensity width 2.5°C and width at quarter  
peak height 5°C.

### Example 8

Example 6 was repeated, but the polymerization temperature was 50°C, the hydrogen content in the gas space was 2.5% by volume and the metallocenes used were 2.5 mg of  
5  $\text{Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$  and 95 mg of phenyl(methyl)silyl(indenyl) $_2\text{HfCl}_2$ . 18.5 kg of polymer were obtained. The extruded molding composition had the following data:

VI = 166  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 45.8 dg/min;  
10  $M_w = 232,000 \text{ g/mol}$ ;  $M_w/M_n = 3.3$ ; melting range maximum at 156°C, shoulder at 140°C, half-intensity width 13°C, width at quarter peak height 30°C; crystallization peak maximum 115°C, width at quarter peak height 8°C.

The molding composition was separated into two constituents semi-quantitatively by fractional crystallization.  
15

Polymer 1 made up about 60% by weight and had the following properties:

VI = 132  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 98 dg/min;  
20  $M_w = 146,000 \text{ g/mol}$ ;  $M_w/M_n = 2.2$ ; melting point 137°C, half-intensity width 7.5°C; crystallization peak 99°C; half-intensity width 6.5°C.

Polymer 2 made up about 40% by weight and had the following data:

VI = 227  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 23 dg/min;  
25  $M_w = 265,500 \text{ g/mol}$ ;  $M_w/M_n = 2.0$ ; melting point 160°C, half-intensity width 5.5°C, width at quarter peak height 6°C; crystallization peak 118°C; half-intensity width 3.5°C, width at quarter peak height 5°C.

### Example 9

30 Example 6 was repeated, but the polymerization temperature was 50°C, the hydrogen content of the gas space was 1.2% by volume and the metallocenes used were 7.5 mg of

$\text{Me}_2\text{Si}(2\text{-methyl-1-indenyl})_2\text{ZrCl}_2$  and 80 mg of  $\text{Me}_2\text{Si}(\text{indenyl})_2\text{HfCl}_2$ . 22.5 kg of polymer were obtained, and the extruded molding composition had the following data:

- 5 VI = 130  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 110 dg/min;  
 $M_w = 142,500 \text{ g/mol}$ ;  $M_w/M_n = 2.0$ ; melting range maximum 149.5°C, shoulder at 137°C, half-intensity width 15.5°C, width at quarter peak height 27.5°C; crystallization peak maximum 112°C, half-intensity width 7.5°C.
- 10 The molding composition was separated semi-quantitatively into two different constituents in a ratio of about 50:50% by weight by fractional crystallization. Of these, polymer 1 had the following data:

- 15 VI = 130  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 114 dg/min;  
 $M_w = 135,000 \text{ g/mol}$ ;  $M_w/M_n = 1.9$ ; melting point 151°C, half-intensity width 8.5°C; crystallization peak 109°C, half-intensity width 5.5°C.

Polymer 2 is characterized as follows:

- 20 VI = 136  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 100 dg/min;  
 $M_w = 142,500 \text{ g/mol}$ ;  $M_w/M_n = 2.2$ ; melting point 135°C, half-intensity width 7°C; crystallization peak 97°C, half-intensity width 6.5°C.

#### Example 10

- 25 The procedure was as in Example 7, but the ratio between the two metallocenes used was changed from 7.5 mg/2.5 mg to 10.4 mg/1.8 mg.

The molding composition obtained after extrusion had the following properties:

- 30 VI = 192  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 30.4 dg/min;  
 $M_w = 241,500 \text{ g/mol}$ ;  $M_w/M_n = 2.3$ ; melting range maximum at 155°C, half-intensity width 12°C, width at quarter peak height 22.5°C; crystallization at 113°C.

### Example 11

The procedure was as in Example 7, but the ratio between the two metallocenes used was changed from 7.5 mg/2.5 mg to 3.9 mg/5.2 mg.

- 5 The molding composition obtained after extrusion had the following properties:

VI = 197 cm<sup>3</sup>/g; MFI (230/5) = 28.9 dg/min;  
M<sub>w</sub> = 214,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.5; melting range maximum at  
10 158°C, width at quarter peak height 24°C; crystallization  
at 116°C.

### Example 12

The procedure was as in Example 8, but the ratio between the two metallocenes used was changed from 2.5 mg/95 mg to 1.5 mg/125 mg.

- 15 The molding composition examined after extrusion had the following properties:

VI = 162 cm<sup>3</sup>/g; MFI (230/5) = 62 dg/min;  
M<sub>w</sub> = 198,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.7; melting range maximum at  
151°C, shoulder at 135°C, half-intensity width 16°C,  
20 width at quarter peak height 32.5°C; crystallization at  
114°C.

### Example 13

The procedure was as in Example 8, but the ratio between the two metallocenes used was changed from 2.5 mg/95 mg  
25 to 3.6 mg/51.5 mg.

The molding composition examined after extrusion had the following properties:

VI = 187 cm<sup>3</sup>/g; MFI (230/5) = 37.1 dg/min;

$M_w = 209,500$  g/mol;  $M_w/M_n = 2.9$ ; melting range maximum at  $157^\circ\text{C}$ , width at quarter peak height  $27.5^\circ\text{C}$ ; crystallization at  $116^\circ\text{C}$ .

#### Example 14

5 A dry  $24\text{ dm}^3$  reactor was flushed with propylene and charged with  $10\text{ dm}^3$  (S.T.P.) of hydrogen,  $12\text{ dm}^3$  of liquid propylene and  $32\text{ cm}^3$  of a toluene solution of methylaluminumoxane (corresponding to  $52\text{ mmol}$  of Al, mean degree of oligomerization  $n = 21$ ). The contents were stirred at  
10  $30^\circ\text{C}$  for 15 minutes at 250 rpm.

In parallel,  $6.2\text{ mg}$  of rac-ethylene(2-methyl-1-indenyl) $_2\text{ZrCl}_2$  and  $1.0\text{ mg}$  of rac- $\text{Me}_2\text{Si}$ (2-methyl-4-phenyl-1-indenyl) $_2\text{ZrCl}_2$  were dissolved in  $12\text{ cm}^3$  of a toluene solution of methylaluminumoxane ( $20\text{ mmol}$  of Al) and pre-  
15 activated by standing for 15 minutes. The solution was introduced into the reactor, and the mixture was polymerized at  $60^\circ\text{C}$  for 1 hour.  $2.05\text{ kg}$  of polypropylene were obtained. The molding composition prepared by extrusion had the following data:

20 VI =  $285\text{ cm}^3/\text{g}$ ; MFI (230/5) =  $7.5\text{ dg/min}$ ;  $M_w = 395,000$  g/mol;  $M_w/M_n = 3.3$ ; melting range maximum  $159^\circ\text{C}$ , shoulder at  $151^\circ\text{C}$ , half-intensity width  $14^\circ\text{C}$ , width at quarter peak height  $30.5^\circ\text{C}$ ; crystallization at  $116^\circ\text{C}$ .

#### 25 Example 15

The procedure was as in Example 14, but no hydrogen was used, the polymerization temperature was  $70^\circ\text{C}$  and the metallocenes used were  $1.8\text{ mg}$  of rac-ethylidene(2-methyl-4,6-diisopropyl-1-indenyl) $_2\text{ZrCl}_2$  and  $2.5\text{ mg}$  of rac-  
X 30  $\text{Me}_2\text{Si}$ (2-methyl-4,5-benzoinindenyl) $_2\text{ZrCl}_2$   <sup>$\text{ZrCl}_2$</sup>   ~~$\text{ZrCl}_2$~~   $2.07\text{ kg}$  of polymer powder were obtained. The molding composition prepared by extrusion had the following data:

VI = 245 cm<sup>3</sup>/g; MFI (230/5) = 8.5 dg/min;  
M<sub>w</sub> = 296,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.9; melting range maximum  
145°C, half-intensity width 16.5°C, width at quarter peak  
height 25.5°C; crystallization at 109°C.

5 Example 16

The procedure was as in Example 15, but the metallocenes  
used were 5.0 mg of dimethylmethylene (9-fluorenyl)-  
(cyclopentadienyl)ZrCl<sub>2</sub> and 5.0 mg of phenyl(methyl)-  
methylene(9-fluorenyl)(cyclopentadienyl)ZrCl<sub>2</sub>. 1.63 kg of  
10 polypropylene were obtained, giving, after extrusion, a  
molding composition having the following properties:

VI = 141 cm<sup>3</sup>/g; MFI (230/5) = 32.5 dg/min;  
M<sub>w</sub> = 125,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.5; melting range maximum at  
125 and 132°C, half-intensity width 24.5°C, width at  
15 quarter peak height 41.5°C; crystallization at 57°C and  
75°C, half-intensity width 31.5°C.

Example 17

A dry 24 dm<sup>3</sup> reactor was flushed with propylene and  
charged with 9.5 dm<sup>3</sup> (S.T.P.) of hydrogen and 12 dm<sup>3</sup> of  
20 liquid propylene. 35 cm<sup>3</sup> of a toluene solution of methyl-  
aluminoxane (corresponding to 52 mmol of Al, mean degree  
of oligomerization n = 20) were then added. In parallel,  
6.5 mg of rac-phenyl(methyl)silyl(2-methyl-4,6-diiso-  
propyl-1-indenyl)<sub>2</sub>ZrCl<sub>2</sub> were dissolved in 13.5 cm<sup>3</sup> of a  
25 toluene solution of methylaluminoxane (20 mmol of Al) and  
preactivated by standing for 5 minutes.

The solution was then introduced into the reactor, and  
the mixture was polymerized at 60°C for 1 hour with  
continuous addition of 60 g of ethylene. 2.59 kg of  
30 random copolymer were obtained. The ethylene content of  
the copolymer was 2.0% by weight.

VI = 503 cm<sup>3</sup>/g; M<sub>w</sub> = 384,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.0; melting



point = 139°C.

A second polymerization was carried out in the same way, but with 5 dm<sup>3</sup>(S.T.P.) of hydrogen and without addition of ethylene. The metallocene used was 2.5 mg of rac-dimethylsilyl(2-methyl-4-phenyl-1-indenyl)<sub>2</sub>ZrCl<sub>2</sub>. 1.71 kg of polypropylene were obtained.

VI = 524 cm<sup>3</sup>/g; M<sub>w</sub> = 448,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.0; melting point = 162°C.

1.5 kg of each of the polymers obtained in the two polymerization reactions were stabilized against chemical degradation under extrusion conditions by means of 6 g of pentaerythrityl tetrakis[3-(3,5-di-t-butyl-4-hydroxy-phenyl)propionate], extruded in a ZSK 28 twin-screw extruder (Werner und Pfleiderer) and subsequently granulated. The temperatures in the heating zones were 150°C (feed), 250°C, 270°C, 270°C and 270°C (die plate), the material temperature was 285°C and the extruder screws rotated at 150 rpm.

The molding composition prepared in this way had the following properties:

VI = 548 cm<sup>3</sup>/g; M<sub>w</sub> = 424,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.5; melting range maximum 158°C, shoulder at 143°C, half-intensity width 19.5°C, width at quarter peak height 35.5°C; crystallization at 119°C, half-intensity width 11.5°C.

#### Example 18

The procedure was as in Example 14, but the second metallocene used instead of rac-Me<sub>2</sub>Si(2-methyl-4-phenyl-1-indenyl)<sub>2</sub>ZrCl<sub>2</sub> was the compound Ph(Me)Si(2-methyl-4-phenyl-1-indenyl)<sub>2</sub>ZrCl<sub>2</sub>.

1.95 kg of polypropylene were obtained. The extruded molding composition had the following data:

VI = 325 cm<sup>3</sup>/g; MFI (230/5) = 3.9 dg/min; melting range maximum 160°C, shoulder at 150°C, half-intensity width

16°C, width at quarter peak height 31°C; crystallization at 114°C.

#### Example 19

The procedure was as in Example 14, but the second  
5 metallocene used instead of  $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$  was the compound  $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-(1-naphthyl)-1-indenyl})_2\text{ZrCl}_2$ . 2.55 kg of polypropylene were obtained. The extruded molding composition had the following data:  
10 VI = 419  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 0.9 dg/min; melting range maximum 162°C, shoulder at 150°C, half-intensity width 18°C, width at quarter peak height 30°C; crystallization at 110°C.

#### Example 20

15 The procedure was as in Example 14, but the metallocenes used were 4.0 mg of  $\text{rac-Me}_2\text{Si}(2,5,6\text{-trimethyl-1-indenyl})_2\text{-ZrCl}_2$  and 0.8 mg of  $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-(1-naphthyl)-1-indenyl})_2\text{ZrCl}_2$ . 2.30 kg of polypropylene were obtained. The extruded molding composition had the following data:  
20 VI = 379  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 3.0 dg/min; melting peak maximum 161°C, shoulder at 137°C, half-intensity width 22°C, width at quarter peak height 35°C; crystallization at 112°C.

#### Example 21

25 The procedure was as in Example 14, but the metallocenes used were 3.0 mg of  $\text{rac-Me}_2\text{Si}(4,5\text{-benzo-1-indenyl})_2\text{ZrCl}_2$  and 0.8 mg of  $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-(1-naphthyl)-1-indenyl})_2\text{ZrCl}_2$ . 2.10 kg of polypropylene were obtained. The extruded molding composition had the following data:  
30 VI = 225  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 23.5 dg/min; melting peak maximum 161°C, shoulder at 140°C, half-intensity width 17°C, width at quarter peak height 32°C; crystallization at 111°C.

Example 22

The procedure was as in Example 14, but the metallocenes used were 6.0 mg of  $\text{rac-Me}_2\text{Si}(4\text{-phenyl-1-indenyl})_2\text{ZrCl}_2$  and 0.8 mg of  $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$ . 2.23 kg of polypropylene were obtained. The extruded molding composition had the following data: VI = 220  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 25 dg/min; melting peak maximum 160°C, shoulder at 149°C, half-intensity width 15°C, width at quarter peak height 30°C; crystallization at 115°C.

Example 23

The procedure was as in Example 22, but in addition 70 g of ethylene were metered continuously into the reactor during the 1-hour polymerization time. 2.35 kg of ethylene/propylene copolymer were obtained. VI = 190  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 45 dg/min; melting peak maximum 148°C, shoulder at 132°C, half-intensity width 14°C. The copolymer contained 2.5% by weight of ethylene distributed randomly.

Comparative Example 1

The procedure was as in Example 1, but the following polymers were used:

Polymer 1: VI = 230  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 15 dg/min;  $M_w = 268,000 \text{ g/mol}$ ;  $M_w/M_n = 2.0$ ; melting point (maximum) 157°C, half-intensity width of the melting peak 7°C; width at quarter peak height 10°C; crystallization point 112°C.

Polymer 2: VI = 235  $\text{cm}^3/\text{g}$ ; MFI (230/5) = 12 dg/min;  $M_w = 272,000 \text{ g/mol}$ ;  $M_w/M_n = 2.1$ ; melting point (maximum) 154°C, half-intensity width of the melting peak 8°C; width at quarter peak height 12°C; crystallization point 109°C, width of crystallization peak (at quarter peak

height) 5°C.

#### Comparative Example 2:

The procedure was as in Example 1, but the following polymers were used:

- 5 Polymer 1: VI = 260 cm<sup>3</sup>/g; MFI (230/5) = 5 dg/min; M<sub>w</sub> = 295,000 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.3; melting point (maximum) 149°C, half-intensity width of the melting peak 6°C; width at quarter peak height 13°C; crystallization point 106°C.
- 10 Polymer 2: as polymer 2 in Example 1

The non-novel molding composition prepared by extrusion had the following data:

- VI = 249 cm<sup>3</sup>/g; MFI (230/5) = 8 dg/min; M<sub>w</sub> = 294,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.6; melting point (maximum) 151°C, half-intensity width of the melting peak 8°C; width at quarter peak height 12°C; crystallization point 105°C.
- 15

#### Comparative Example 3

- The procedure was as in Example 1, but the following polymers were used:
- 20

Polymer 1: as polymer 1 in Example 1.

- Polymer 2: VI = 230 cm<sup>3</sup>/g; MFI (230/5) = 14 dg/min; M<sub>w</sub> = 274,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.3; melting point (melting peak maximum) 135°C, half-intensity width of the melting peak 5.5°C; width at quarter peak height 14°C; crystallization point 102°C.
- 25

The non-novel molding composition prepared by extrusion had the following data:

VI = 240 cm<sup>3</sup>/g; MFI (230/5) = 12 dg/min;  
M<sub>w</sub> = 287,500 g/mol; M<sub>w</sub>/M<sub>n</sub> = 2.4; melting point (maximum)  
137°C, half-intensity width of the melting peak 5.5°C;  
width at quarter peak height 14°C; crystallization point  
5 102°C, half-intensity width of the crystallization peak  
4°C, width at quarter peak height 5°C.